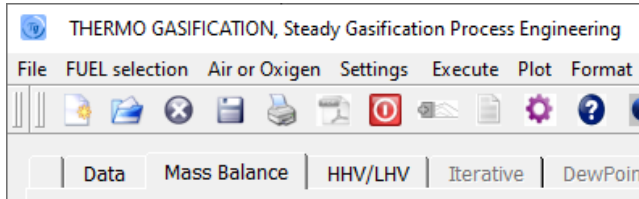




THERMO GASIFICATION | Technical & Educational Software



THERMOGasification is a software for the thermodynamic analysis of the thermochemical process in which the reactions between fuel and the gasification agent take place and syngas (product gas, synthetic gas, or synthesis gas) is produced. THERMOGasification is at the forefront of thermal technology, offering innovative and efficient thermal energy solutions applied to the gasifier.

INDEX

Characteristics

- **Solid technology**
- **Precision**
- **Easy handling**
- **Intuitive interface**
- **Input variability**
- **Application in several industrial systems**

Software capabilities

- Thermo-chemical analysis
- Mass, energy and exergetic balance
- Energetic flow and *Grassmann* diagram
- Thermal and exergetic efficiency
- Sensitivity analysis
- Pollutant emissions control

Applications

- Production of fuel for use in electric power generation units.
- Manufacturing synthetic or substitute natural gas for use as pipeline gas supplies.
- Producing hydrogen for fuel cell applications.
- Production of synthesis gas for use as a chemical feedstock.
- Generation of fuel gas (low-Btu or medium-Btu gas) for industrial purposes.

Characteristics

Software algorithms are based on up-to-date bibliography and the latest mathematical models, which in conjunction result in a **well-defined** and **solid technology**. The software has been set up with an **intuitive interface** that allows **easy handling**.

Input data (fuel)

The demand for energy sources to satisfy human energy consumption continues to increase. Prior to the use of fossil fuels, biomass was the primary source of energy for heat via combustion.

FUEL selection

- Gasification of Solid Fuel
 - Gasification of Biomass
 - Steam Reforming of Methane
 - Steam Reforming of Methanol
 - Steam Reforming of Natural Gas

Anthracite
Solid Fuel Composition
Anthracite
Bituminous Coal
Semi-Bituminous Coal
Charcoal
Coke
Fat Coal
Gas Flame Coal
Biomass Composition
Biomass Composition
Almond shells
Casuarina wood
Coconut shell
Corn stover
Cotton gin trash
Deoiled bran
Grape pomace
Grape stalks
Hybrid poplar



Natural Gas

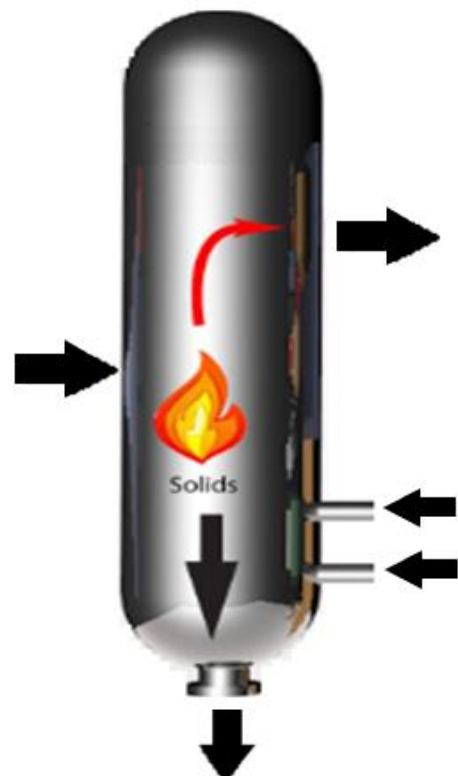
Molar Analysis

Molar ratio %	
92.0000	Methane
4.0000	Ethane
2.0000	Propane
0.6000	nButane
0.4000	nPentane
0.5000	CO2
0.5000	N2

Fuel selection features

Application in industrial systems

The main operating parameters of the gasifier include type and design of gasifier, gasification temperature, flow rates of biomass and oxidizing agents (air or steam), type and amount of catalysts, and biomass type and properties. Gasification takes place at high temperature in the presence of an oxidizing agent. Char and tar are the result of incomplete conversion of biomass.



Gasifier (for biomass or coal)

Thermo-chemical analysis

As a first step, a **mass balance** of combustion products can be obtained. Strict analysis on whole range of **fuel properties**: calorific powers, specific heat, enthalpy of formation, chemical exergy and entropy.

FUEL COMPOSITION

Molar Analysis		Ultimate Analysis		FUEL DATA	
mol/kg fuel	Molar ratio %	Mass ratio %			
77.179	80.623	92.7000	C	CARBON	
17.362	18.137	3.5000	H ₂	HYDROGEN	
			N ₂	NITROGEN	
0.843	0.881	2.7000	O ₂	OXYGEN	
0.343	0.358	1.1000	S	SULPHUR	
			H ₂ O	MOISTURE	
			ASH		

100.0000 Total (%) As fired (wet, ash)

FLUE GAS On wet basis On dry basis

	mol/mol fuel	kg/kg fuel	Mole %	Mass %
CO ₂	0.03633	0.15304	2.1952	4.5746
CO	0.28550	0.76552	17.2508	22.8828
H ₂ O	0.01481	0.02555	0.8949	0.7637
H ₂	0.15947	0.03077	9.6357	0.9198
N ₂	0.67086	1.79903	40.5353	53.7762
SO ₂	0.00072	0.00439	0.0435	0.1312
H ₂ S	0.00286	0.00934	0.1728	0.2792
O ₂				
CH ₄	0.00213	0.00327	0.1287	0.0977
C(s)	0.48228	0.55452	29.1408	16.5756
TOTAL	1.6550	3.3454	100.00 %	100.00 %

With the definition of fuel composition by means of an ultimate analysis, or the carbon, hydrogen, oxygen, nitrogen, sulphur, ash and water is possible the modelling for different types of fuel. It is also possible to define a mixture of hydrocarbons for a natural gas.

Mass balance interface

Mathematical model

The chemistry of gasification is quite complex and is accomplished through a series of physical transformations and chemical reactions within the gasifier: Water-gas, steam reforming, combustion, Boudouard, water-gas-shift and methanation.

Within the gasification process, the chemical reactions of gasification can progress to different extents depending on the gasification conditions and the feedstock used. The main steps involved in the gasification process can be categorized as upstream processing, gasification and downstream processing.

Equilibrium equations: Gumz (1950)

Boudouard reaction
 $C + CO_2 \rightleftharpoons 2CO$

Water-gas reaction
 $C + H_2O \rightleftharpoons CO + H_2$

Methanation
 $C + 2H_2 \rightleftharpoons CH_4$

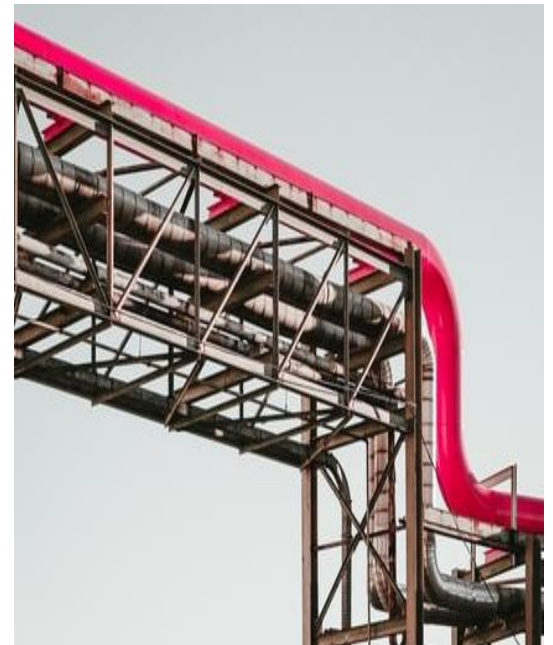
Equilibrium constant	Dissociation
1.91339	0.0183746
2.62066	0.0450569
0.09821	0.0026415

Equilibrium equations:

Steam reforming reaction
 $CH_4 + H_2O \rightleftharpoons 3H_2 + CO$

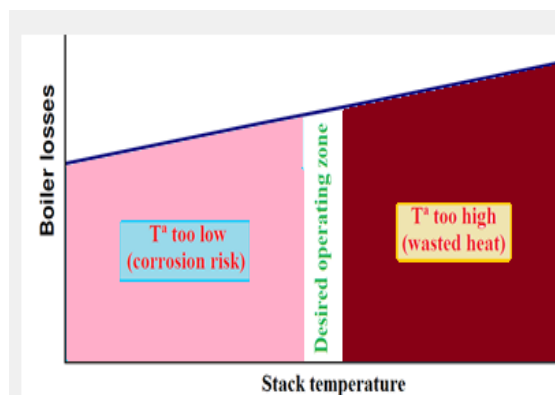
Water gas shift reaction
 $CO + H_2O \rightleftharpoons CO_2 + H_2$

Equilibrium constant	Dissociation
27.6069	0.973991
1.4353	0.292



Sulfuric acid dew point

To prevent sulfuric acid condensation problems in industrial facilities that burn fuels with the presence of sulfur, it is necessary to know the dew point temperature of the sulfuric acid. An exhaustive analysis of the chemical reactions involved until reaching the formation of sulfuric acid is carried out.



Correlations:

- Okkes(1987)
- Verhoff / Banchero (1974)**
- Haase / Borgmann (1981)
- Okkes(1987)
- Kiang (1981)
- ZareNezhad (2009)
- Blanco / Peña (2008)

Okkes(1987)

Dew Temperature: 97.49 °C

Fuel characterization

Includes different properties of the fuel for each type of fuel: biomass, coal, natural gas, methane, methanol, etc.

Properties of the FUEL

CH (weight)	HC (atomic)
<input type="text" value="71.253"/> kg C/kg H	<input type="text" value="0.450"/> mol H/mol C
Oxygen content	Carbon content
<input type="text" value="0.0270"/> kg O ₂ /kg fuel	<input type="text" value="0.9270"/> kg C/kg fuel

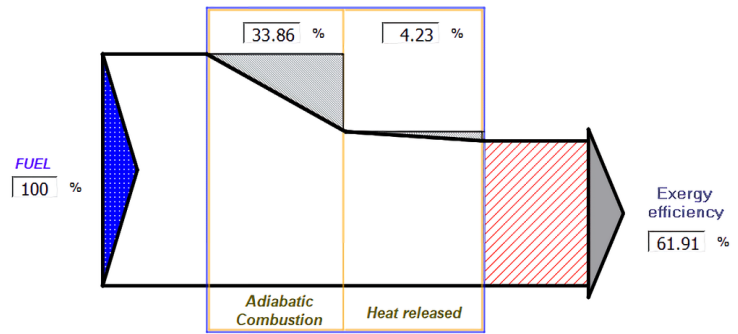
Properties of the fuel (biomass, coal, natural gas, methane, methanol, etc)

Lower Heating, LHV	Higher Heating, HHV
NET	GROSS
<input type="text" value="372.90"/> kJ/mol fuel	<input type="text" value="380.93"/> kJ/mol fuel
<input type="text" value="35696.70"/> kJ/kg fuel	<input type="text" value="36465.30"/> kJ/kg fuel
<input type="text" value="kJ/mol & kJ/kg"/>	

Heat of combustion of the fuel

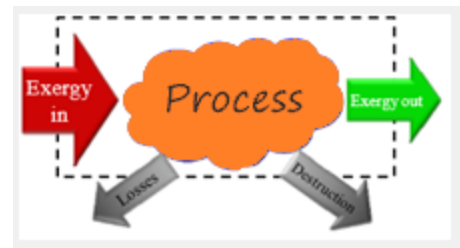
Exergy analysis

Based on Second Principle, it provides information about **irreversibilities** generated in each device of the installation, including the internal of the all the process.



Results visualization using a Grassmann combustion diagram

From second law evaluations (entropy or exergy evaluations) it is generally known that thermodynamic losses of boilers and furnaces are much higher than the thermal efficiencies do suggest.



Exergy flow diagram

Syngas production

It provides the different categories of gasification reactors as they apply to various types of feedstocks. In terms of feedstock variability, several different types of feedstocks that vary widely in composition are available for gasification and include crude oil residues, coal, wood, wood waste as well as a multitude of agricultural residues, domestic waste, and industrial waste.

Lower Heating, LHV (syngas)

SYNGAS

<input type="text" value="7654.13"/> kJ/kg	<input type="text" value="610.18"/> kJ/m ³
<input type="text" value="163.04"/> kJ/mol	

Energy Balance (25 °C, 1 atm)

Experimental correlations

Heat of combustion of the syngas

Pollutant emissions control

Includes critical pollutants as carbon monoxide (CO), methane (CH₄) or sulfur dioxide (SO₂) among others (CO₂).

Syngas production efficiency

$$\eta = \frac{N_{H_2} LHV_{H_2} + N_{CO} LHV_{CO}}{Q_{reactor} + N_{coal} LHV_{coal}}$$

°C
 kPa

%

Product Temperature

(Stack Temperature)

°C

Adiabatic Temperature

°C

The increase in gasification temperature gives rise to an increase in gas formation and a subsequent decrease in tar and char yields. Temperature also has an effect on the gas composition. The rise in temperature usually gives rise to an increase in H₂ and a decreased in CO and light hydrocarbons. Nevertheless, thermodynamic models have shown that a smooth decrease in H₂ yield occurs at very high reaction temperatures.

Emission factors (LHV)

CO₂	<input type="text" value="0.045"/> kg/kWh
	<input type="text" value="12.540"/> kg/GJ
H₂O	<input type="text" value="0.012"/> kg/kWh
	<input type="text" value="3.219"/> kg/GJ
CH₄	<input type="text" value="0.002"/> kg/kWh
	<input type="text" value="0.634"/> kg/GJ
SO₂	<input type="text" value="0.000"/> kg/kWh
	<input type="text" value="0.023"/> kg/GJ

Pollutant emissions

Applications

The gasification of the biomass implies an incomplete combustion that results in the production of combustible gases (syngas) consisting of carbon monoxide (CO), hydrogen (H₂) and traces of methane (CH₄). This mixture is called producer gas. The producer gas can be used to run internal combustion engines (both compression and spark ignition), can be used to power furnaces in direct heat applications and can be used to produce, in an economically viable manner, methanol, which is useful both as fuel for thermal engines and for chemical raw materials for industries.

Since any biomass material can undergo gasification, this process is much more attractive than the production of ethanol or biogas, where only selected biomass can produce these fuels. In addition, since solid waste is seldom in a form that can be easily used economically, it is advantageous to convert this waste into a more easily usable fuel from a similar producer gas. Hence the attraction of gasification.

Academia application specifications

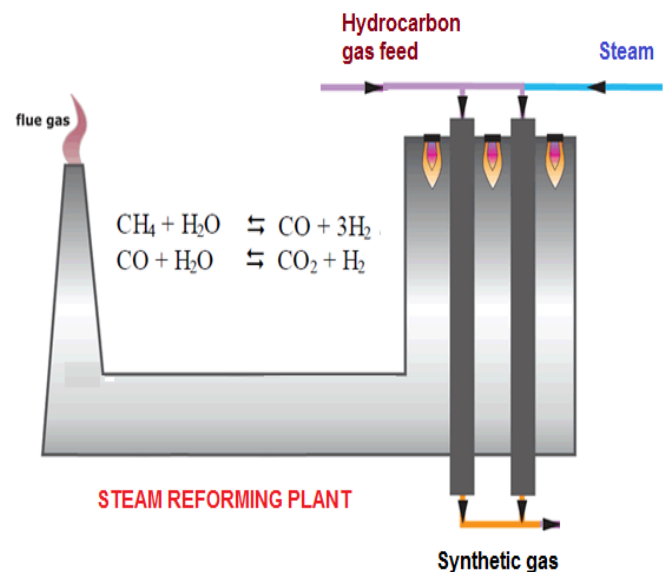
This software's capabilities are appropriate for gasification studies in academia. Major application for process optimization in industry or equilibrium-chemical processes study in **academia**.

Enthalpy of the products			Entropy of the products		
	kJ/mol	kJ/kg fuel		J/mol K	kJ/kg fuel K
CO ₂	-360.069	-1616.774	CO ₂	200.860	0.902
CO	-88.829	-2384.654	CO	158.854	4.265
H ₂ O	-215.814	-607.773	H ₂ O		
H ₂	20.694	477.224	H ₂	154.339	3.559
N ₂	21.476	558.797	N ₂	158.853	4.133
CH ₄	-36.363	-22.640	O ₂		
SO ₂	-262.408	-1.490	SO ₂	238.280	0.001
H ₂ S	7.454	0.169	H ₂ S	214.911	0.005
O ₂			Ar		
Ar			CH ₄	195.648	0.122
TOTAL	-913.859	-3597.141	TOTAL	1321.745	12.987

Thermodynamic properties for each specie of the syngas



Methane steam reforming is the most common and cost-effective method for hydrogen production, and it contributes about 50% of the world's hydrogen production. First stage is the steam reforming of methane. Second stage is the water-gas shift process. Steam methane reforming is a process requiring high temperature and pressure. During the process, hydrogen is generated in reactions and with methane/CO and water participation under pressure.



Methane steam reforming installation